

In The Name of God

Mathematical Modeling of Fluid Flow and Particle Movement in Electrostatic Precipitators

By
Mohammadreza Talaie Khoozani

Thesis

Submitted to the School of Graduate studies in Partial Fulfillment of the Requirements for the Degree of Doctor of Philosophy (Ph.D.)

In
Chemical Engineering
Shiraz University
Shiraz, Iran

Evaluated and approved by the Thesis Committee as: Excellent

.....*M. Taheri*..... M. Taheri, Ph.D., Professor
of Chemical Engineering (Chairman)

.....*J. Fathikalajahi*..... J. Fathikalajahi, Ph.D., Professor
of Chemical Engineering (Chairman)

.....*A. Jahanmiri*..... A. Jahanmiri, Ph.D., Assoc. Prof.
of Chemical Engineering

.....*H. Abiri*..... H. Abiri, Ph.D., Assoc. Prof.
of Electrical Engineering

.....*B. Dabir*..... B. Dabir, Ph.D., Professor
of Chemical Engineering
(Amirkabir University)

June 2000

۳/۳۰/۱

To My Wife, Parents and Family

And

To All Who Teach Me

Acknowledgement

I would like to express my special thanks and gratitude to Professors J. Fathikaljahi and M. Taheri for supervising and supporting this investigation during my Ph.D. course. Also, I would like to thank Professors A. Jahanmiri and H. Abiri for their valuable contribution as committee members of this thesis and Professor B. Dabir as invited referee for his valuable suggestions and recommendations. Also I wish to thank Professor J. Raper and P. Bahri for their help during my 9-month stay at Sydney University and Murdoch University in Australia.

Abstract

Mathematical Modeling of Fluid Flow and Particle Movement in Electrostatic Precipitators

By

Mohammadreza Talaie Khoozani

A mathematical model was developed to evaluate the electrostatic precipitator performance and investigate the effect of various parameters on the particle removal efficiency. This model consists of three interactive sections, namely electrical field, gas flow and turbulence and particle movement predictions. Two kinds of ESP single-stage and double-stage were considered and due to ESP's configuration the governing equations were obtained for two-dimensional case. In order to evaluate the electrical conditions of an ESP the Maxwell's relation was used. A new model was developed to calculate the electrical conditions of a single-stage ESP. this model is capable of evaluating corona sheath growth and ionic current for different values of applied voltages. The gas flow field was determined by using the normal k- ϵ turbulent model with considering electrical body force due to presence of ions and charged particles. SIMPLER algorithm was applied to solve the Navier-stokes, continuity, k and ϵ equations. The particle movement was evaluated by using two different methods of

Eulerian and Lagrangian. Both methods were modified for considering the effect of particle size distribution on the ESP performance. The effect of applied voltage, particle diameter, particle size distribution, inlet particle concentration, configuration of ESP's channel and baffles were investigated on the ESP performance.

Table of Contents

Content	Page
List of Tables	X
List of Figures	XI
Nomenclature	XVIII
Chapter 1: Introduction	1
Chapter 2: Literature review	8
2.1 Electrical field investigations	19
Chapter 3: Introduction to mathematical model	25
3.1 Introduction	25
3.2 Parameters affecting on ESP process	27
Chapter 4: Electrical field	31
4.1. Introduction	31
4.2 Governing equations	32
4.3 Method of solution and boundary conditions	33
4.3.1 Double-stage electrostatic precipitators	33
4.3.2 Single-stage electrostatic precipitators	36
4.4 Comparison between the present model and the previous ones	40
4.5 Results	41

4.6 Conclusion	49
Chapter 5: Fluid flow	50
5.1 Introduction	50
5.2 k- ϵ turbulent model	52
5.3 Governing equations and boundary conditions	54
5.3.1 Wall function	56
5.4 Method of solution	59
5.4.1 x-component momentum equation	60
5.4.1.1 Control volumes adjacent to a horizontal wall	63
5.4.1.2 Control volume at left-hand corner of a block	65
5.4.1.3 Control volume at right-hand corner of a block	70
5.4.2 y-component momentum equation	72
5.4.2.1 Control volumes adjacent to a vertical wall	74
5.4.2.2 Control volume at left-hand corner of a block	76
5.4.2.3 Control volume at right-hand corner of a block	80
5.4.3 Kinetic energy (k) equation	82
5.4.3.1 Control volumes adjacent to a wall	85

5.4.4 Kinetic energy dissipation rate (ϵ) equation	86
5.4.4.1 Control volumes adjacent to a wall	88
5.4.5 Continuity equation	90
5.4.5.1 velocity correction equations	91
5.4.5.2 Pressure correction equations	92
5.4.5.3 Pressure equation	93
5.5 Body force	95
5.6 Results	96
5.6.1 Fluid velocity field without considering ion flow	96
5.6.2 Fluid velocity field with considering ion flow	98
5.7 Conclusion	103
Chapter 6: Particle movement	104
6.1 Introduction	104
6.2 Eulerian approach	106
6.2.1 Method of solution	109
6.2.2 Results	112
6.3 Lagrangian approach	133
6.3.1 Results	137
Chapter 7: Conclusions and recommendations	141
Appendix A: Finite volume method	144
Appendix B: Grid generation	162

Appendix C: Derivation of dimensionless number N_{Ta}	171
References	173
Abstract and title page in Persian	

List of Tables

Content	Page
Table 1-1 The description of several investigations about fluid flow field in ESPs	22
Table 1-2 The description of several investigations about electrical field in ESPs	23
Table 1-3 The description of several investigations about particle movement in ESPs	24
Table 5-1 The empirical constants used in normal k- ϵ turbulent flow model	55
Table 5-2 The boundary conditions of the equations governing flow field	55
Table 5-2 Definitions of Γ and S for governing equations	60
Table 5-3 The conditions of the experimental data of Good and Joubert (1968) for the recirculation length created behind of a thin rib and Crabb et al. (1977) for recirculation length behind of a square rib	97
Table 5-4 The comparison of the experimental and theoretical values of recirculation lengths	98
Table 6-1 The comparison of advantages and disadvantages of Eulerian and Lagrangian approaches	105

List of Figures

Content		Page
Figure 1-1	Single-stage cylindrical electrostatic precipitator	6
Figure 1-2	The schematic figure of a single-stage wire-plate electrostatic precipitator	7
Figure 3-1	Simple configurations of single-stage and double stage ESPs	26
Figure 3-2	The structure of collective electrode in single-stage and double stage ESP	26
Figure 3-3	The parameters affecting on particle removal efficiency and their interactions	30
Figure 4-1	The control volume used for discretizing electrical potential equation	34
Figure 4-2	Demonstrative scheme of the control volume surrounding a wire	39
Figure 4-3	Current-voltage characteristics curve, comparison between the results and experimental data reported by Cooperman (1981). Wire diameter: 2.768×10^{-3} m. wire-plate distance: 0.1524 m. wire-wire distance: 0.1524 m. positive corona	44
Figure 4-4	Current-voltage characteristics curve, comparison between the results and experimental data reported by Cooperman (1981). Wire diameter: 1.778×10^{-4} m. wire-plate distance: 0.2286 m. wire-wire distance: 0.2286 m. positive corona	44

- Figure 4-5** Current-voltage characteristics curve, comparison between the results and experimental data of Penny and Matick (1960).
Wire-plate distance: 0.1143 m, wire-wire distance: 0.14696 m and negative corona 45
- Figure 4-6** Current-voltage characteristics curve, comparison between the results and experimental data of Penny and Matick (1960).
Wire-plate distance: 0.1143 m, wire-wire distance: 0.14696 m and negative corona 45
- Figure 4-7** Current-voltage characteristics curve, comparison between the results and experimental data of Penny and Matick (1960).
Wire-plate distance: 0.1143 m, wire-wire distance: 0.14696 m and negative coron 46
- Figure 4-8** Current-voltage characteristics curve, comparison between the results and experimental data of McDonald et. al (1977).
Wire diameter: 1.346×10^{-3} m. Wire-plate distance: 0.0635m, wire-wire distance: 0.127 m and negative corona 46
- Figure 4-9** Comparison between the calculated current-voltage characteristic curves of negative and positive corona. Wire diameter: 1.0×10^{-3} m, Wire-plate distance: 0.1m and wire-wire distance: 0.1 m 47
- Figure 4-10** The profile of electrical potential along a line from wires to the plate, comparison between the results and experimental data of Penny and Matick (1960).
Wire diameter: 2.768×10^{-3} m, wire-plate distance: 0.1143 m, wire-wire distance: 0.14696 m, applied voltage: 80 kV and negative corona 47
- Figure 4-11** Comparison between the calculated corona radius augmentations of negative and positive corona. Wire

	diameter: 1.0×10^{-3} m, Wire-plate distance: 0.1m and wire-wire distance: 0.1 m	48
Figure 4-12	The effect of a uniform particle charge on current-voltage characteristics curve. Wire diameter: 2.768×10^{-3} m. wire-plate distance: 0.1524 m. wire-wire distance: 0.1524 m. positive corona	48
Figure 5-1	A typical staggered-system control volume for deriving the discretized form of x-component momentum equation	62
Figure 5-2	The control volume adjacent to a horizontal wall	63
Figure 5-3	The control volume at left-hand corner of a block	66
Figure 5-4	The control volume at right-hand corner of a block	70
Figure 5-5	A typical staggered-system control volume for deriving the discretized form of y-component momentum equation	74
Figure 5-6	The control volume adjacent to a vertical wall	75
Figure 5-7	The control volume at left-hand corner of a block	77
Figure 5-8	The control volume at right-hand corner of a block	80
Figure 5-9	The control volume adjacent to a horizontal wall	84
Figure 5-10	The control volume adjacent to a vertical wall	85
Figure 5-11	The contour plot of gas flow streamline, simulation of Good and Joubert (1968) experiment	99
Figure 5-12	The contour plot of gas flow streamline, simulation of Crabb et al. (1977) experiment	99
Figure 5-13	The contour plot of gas flow streamline for $u_0=0$	100
Figure 5-14	The contour plot of gas flow streamline for $u_0=0.2$ (m/s)	100
Figure 5-15	The contour plot of gas flow streamline for $u_0=0.5$ (m/s)	101
Figure 5-16	The contour plot of gas flow streamline for $u_0=1.0$ (m/s)	101
Figure 5-17	The contour plot of gas flow streamline for $u_0=2.0$ (m/s)	102

Figure 5-18	The contour plot of gas flow streamline for $u_0=3.0$ (m/s)	102
Figure 6-1	Flow chart of solution of governing equations for double-stage ESP	110
Figure 6-1	Schematic configuration of the ESP used in Leonard (1982) experiment	115
Figure 6-2	The result of simulation of fluid flow for Leonard (1982) experiment	116
Figure 6-3	The comparison between the calculated results and experimental data of Leonard (1982)	116
Figure 6-4	The comparison between the trajectories obtained based on unsteady particle momentum equations (-----) and proposed procedure (___) for $D_p=30 \mu\text{m}$, $\phi_0=15$ kV and $u_0= 1.5\text{m/s}$ and with two successive obstructions	117
Figure 6-5	The comparison between the results of the model with using the present procedure (using drag coefficient relations) and conventional procedure (using Stock's law) for calculation of particle velocity field for $\phi_0=20$ kV, $u_0=1.5$ m/s, $E_{ch}=2.5 \times 10^5$ V/m, $N_{co}=0.185$, $\rho_p=1180$ kg/m ³ and configuration of the ESP the same as shown in figure 6-4	117
Figure 6-6	Variation of particle collection efficiency with inlet mass concentration of particles for $\phi_0=20$ kV, $u_0=1.5$ m/s, $E_{ch}=2.5 \times 10^5$ V/m, $\rho_p=1180$ kg/m ³ and configuration of the ESP the same as shown in figure 6-4	118
Figure 6-7	The profile of y-direction electric field strength vector across the entrance of the ESP for $N_{Ta}=0.185$ $\phi_0=20$ kV, $u_0=1.5$ m/s, $E_{ch}=2.5 \times 10^5$ V/m, $\rho_p=1180$ kg/m ³ and configuration of the ESP the same as shown in figure 6-4	118
Figure 6-8	The effect of particle size distribution on particle removal efficiency for applied voltage of 10000 V, mean gas velocity	

	of 1.5 m/s, particle concentration of 10^{-4} kg/m ³ and the same configuration as shown in figure 6-4	119
Figure 6-9	The effect of particle size distribution on particle removal efficiency for applied voltage of 20000 V, mean gas velocity of 1.5 m/s, particle concentration of 10^{-4} kg/m ³ and the same configuration as shown in figure 6-4	119
Figure 6-10	The effect of input particle size distribution on particle removal efficiency for applied voltage of 30000 V, mean gas velocity of 1.5 m/s, particle concentration of 10^{-4} kg/m ³ and the same configuration as shown in figure 6-4	120
Figure 6-11	Contour plot of gas streamline for a double-stage ESP with ribbon with 0.2 m height at 2.5 m from the entrance	121
Figure 6-12	The cumulative variation of particle removal efficiency with length of the ESP's channel for $D_p = 2 \mu\text{m}$	122
Figure 6-13	The cumulative variation of particle removal efficiency with length of the ESP's channel for $D_p = 5 \mu\text{m}$	122
Figure 6-14	The cumulative variation of particle removal efficiency with length of the ESP's channel for $D_p = 10 \mu\text{m}$	123
Figure 6-15	The cumulative variation of particle removal efficiency with length of the ESP's channel for $D_p = 20 \mu\text{m}$	123
Figure 6-16	The cumulative variation of particle removal efficiency with length of the ESP's channel for $D_p = 30 \mu\text{m}$	124
Figure 6-17	The cumulative variation of particle removal efficiency with length of the ESP's channel for $D_p = 40 \mu\text{m}$	124
Figure 6-18	Contour plot of gas streamline for a double-stage ESP with ribbon with 0.2 m height and 1m length at 2.5 m from the entrance	125
Figure 6-19	Contour plot of gas streamline for a double-stage ESP with ribbon with 0.2 m height and 3m length at 2.5 m from the entrance	126